Simulation of Ammonia Production from Synthesis Gas

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Abstract
Ammonia is a compound of nitrogen and hydrogen with the formula NH$_3$. It is a colorless gas with a characteristic pungent smell. Several processes have been invented for optimum production of ammonia. Now-a-days, Haber process is a mainly process for Ammonia production in which the reaction between nitrogen and hydrogen done in the presence of an iron catalyst to form ammonia. In our work, simulation of ammonia synthesis process is done on Aspen Hysys V8.8. By using 333.1 kmole/h of steams, 100 kmole/hr of nitrogen, we have produced 74.62 kmole/hr ammonia. It has also been found that ammonia production increases with the rise of pressure & mass flow of steam& decrease of the temperature of the feed of nitrogen.

Keywords:
Ammonia, Simulation, Haber

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1. Introduction

Ammonia (NH₃) is one of the largest synthetic chemicals, produced in more than 80 countries. In fact, the synthesis of this world class commodity figures among the greatest achievements of industrial chemistry, after which important processes were developed such as methanol, o xo synthesis, Fischer – Tropsch Process and Reppe reactions. Ammonia is basically produced by the reaction between nitrogen and hydrogen, in a 1:3 stoichiometric ratio. Its production routes are related to the hydrogen production method, being steam reforming the main one. Natural gas and naphtha are the most common hydrocarbon feeds used. Currently, most of the existing and almost all new steam reforming plants use natural gas for feedstock.

The most important note is that the production of Ammonia by steam reforming of natural gas is a somewhat clean operation with no significant environmental problems. On the other hand, the use of heavy feed stocks raises additional environmental issues related to, for instance, particulate emissions from solids handling of the feeds.

Hager (2007) approved that, the need for NH₃ production from abundantly available resources such as natural gas and air came about from the vast population growth following in the wake of the industrial revolution in the 1800s. More mouths to feed demanded increased agricultural output and the answer to this was the large scale application of fertilizers.

Appl, M. (2006) explained that, feedstock for textiles, chemical products and explosives is some of applications of ammonia. Haber-Bosch process is used in most modern NH₃ - plants to produce ammonia from nitrogen and hydrogen which are obtained from air and (mainly) natural gas. These processes are operated with reactor temperatures of 400-500°C and pressures ranging from 100-200 bar with considerable recycle of uncreated synthesis gas.

Williams, J. (2015) explained that, ammonia (NH₃) is the most manufactured industrial chemical in the world per weight. 80% of the annual production of 160 M tons (NH₃) is applied as fertilizer either directly or as other ammonium based products. The huge scale and global knowledge of the Haber-Bosch process implies that the production process has to be optimal in order to remain competitive in a global and established yet fluctuating market. Estimates indicate that the global production capacity of ammonia will increase by more than 15% from 2015 to 2018, possibly lowering the price of ammonia if the demand does not simultaneously grow at the same rate.

Computer based simulation has been popular now-a-days for different chemical engineering purposes. Though our task was to represent production of ammonia in renowned aspen HYSYS software, making some assumptions and using hypothetical reactors we have performed the ammonia production simulation. Though it does not give
the real world performance or the real life production environment, but it can give relief from making wide range of experiment without making the small scale reactors or plant. The simulators are used to evaluate the steady state behavior of the process even though the mutual agreement about the reaction mechanism has not been established and thus the reliability of the results cannot be evaluated. The evaluation of the results will be carried out later when the applicability of the models found from the literature will be studied with the process data.

2. Methodology

Aspen hysys is the market leading process modeling solution that provides large economic benefits throughout the process engineering lifecycle & enables companies to design and bring new plants & reduce capital costs. The process of producing ammonia is simulated in Simulation software Aspen Hysys V 8.8. In this simulation we used Peng-Robinson model fits best to equilibrium process.

2.1 Material & Instrumentation:

<table>
<thead>
<tr>
<th>Material</th>
<th>Synthesis gas</th>
<th>Nitrogen</th>
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<tr>
<td></td>
<td>Hydrogen</td>
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<tr>
<td>Software</td>
<td>Aspen Hysys v 8.8</td>
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2.2 Process Description:

Ammonia is produced in a process known as the Haber process, in which nitrogen and hydrogen react in the presence of an iron catalyst to form ammonia. The hydrogen is formed by reacting natural gas and steam at high temperatures and the nitrogen is supplied from the air. Other gases (such as water and carbon dioxide) are removed from the gas stream and the nitrogen and hydrogen passed at high temperature and pressure to form the ammonia.
2.3 Hydrogen Production:
The reaction of methane with water is used to produce the hydrogen. However, before doing this, all sulfurous compounds must be removed from the natural gas to prevent catalyst poisoning. These are removed by heating the gas to 400 °C and reacting it with zinc oxide:

\[ \text{ZnO} + \text{H}_2\text{S} \rightarrow \text{ZnS} + \text{H}_2\text{O} \]

The gas is sent to the primary reformer for steam reforming, where superheated steam is fed into the reformer with the methane. The gas mixture heated with natural gas and purge gas to 770 °C. At this temperature the methane converted to hydrogen, carbon dioxide and small quantities of carbon monoxide.

\[ \text{CH}_4 + \text{H}_2\text{O} \rightarrow \text{CO} + 3 \text{H}_2 \]
\[ \text{CH}_4 + 2 \text{H}_2\text{O} \rightarrow \text{CO}_2 + 4 \text{H}_2 \]
\[ \text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2 \]

2.4 Removal of Carbon Monoxide:
The water gas shift reaction (CO₂ absorber) is used to convert all carbon mono oxides to carbon dioxides according to the following reaction:

\[ \text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2 \]

2.5 Removal of carbon dioxide:
Removing carbon dioxide & remaining of carbon monoxide is very essential step to prevent the poison of ammonia synthesis reaction.

2.6 Ammonia Production:
Ammonia produced due to catalytic reaction between hydrogen and nitrogen according to the following reaction:

\[ \text{N}_2 + \text{H}_2 \rightarrow \text{NH}_3 \]

3. Result and Discussions
After performing the simulation we have found that the production of ammonia depends on different parameters of the process. So by controlling these parameters optimum ammonia production can be obtained.
From the simulation result we have observed the effect of several parameters on production. Those effects are described in below.
3.1 Mass flow rate of steam
The relation between Mass flow rate of steam & mass flow rate of ammonia product can be easily realized from the plot given below:
From the plot, it is observed that the Mass flow rate of steam is directly proportional to ammonia product so the increases of mass flow rate of steam cause increase of the mass flow rate of produced ammonia.

3.2 Pressure of steam
This parameter can be easily observed from the plot given below:
From the plot, it is observed that the pressure of steam is directly proportional to ammonia product so the increases of pressure of steam cause increase of the mass flow rate of produced ammonia.

3.3 Temperature of steam
From the plot below, it is observed that the temperature of steam is inversely proportional to ammonia product so the increases of pressure of steam cause decrease of the mass flow rate of produced ammonia.

3.4 Molar flow rate of Nitrogen
From the plot below, it is observed that the Molar flow rate of Nitrogen is directly proportional to ammonia product so the Molar flow rate of Nitrogen cause increase of the mass flow rate of produced ammonia.

3.5 Pressure of Nitrogen
This parameter can be easily observed from the plot given below:
From the plot, it is observed that the Pressure of Nitrogen is directly proportional to ammonia product until the pressure reach to $2.754 \times 10^4$ kpa the relation is turned to inversely proportional so in this simulation the optimum operating pressure of Nitrogen is $2.754 \times 10^4$ kpa.

3.6 Temperature of Nitrogen:
This parameter can be easily observed from the plot given below:
From the plot, it is observed that the temperature of Nitrogen is inversely proportional to ammonia product so the increases of temperature of Nitrogen cause decrease of the mass flow rate of produced ammonia.
3.7 Temperature of feed of stream (1) on the duty of cooler (1):
From the plot below, it is observed that the temperature of feed of stream (1) is directly proportional to duty of the cooler so the increase of temperature of feed of stream (1) cause increase of the duty of cooler.

4. Conclusion
Ammonia synthesis is an important chemical process. In our paper, we have generated data based on the simulation performed in HYSYS. This data can help us understand the process in different situation in industrial practice. By varying the different parameters in this simulation environment, the effects of these parameters on ammonia production are observed and the results are shown in graphical form. Using the plots, the optimum conditions for ammonia production can be easily found out.

5. References
Figure (1) block diagram of ammonia plant

Figure (2) Hysys Process Flow diagram of ammonia synthesis
Figure (3): Mass flow rate of steam vs. Mass flow rate of ammonia

Figure (4): pressure of steam vs. Mass flow rate of ammonia
Figure (5): temperature of steam vs. Mass flow rate of ammonia

Figure (6): Mass flow rate of Nitrogen vs Mass flow rate of ammonia
Figure (7): Pressure of Nitrogen vs. Mass flow rate of produced ammonia.

Figure (8): Temperature of Nitrogen vs. Mass flow rate of produced ammonia.
Figure (9): Temperature of stream (1) vs. the duty of cooler (1).